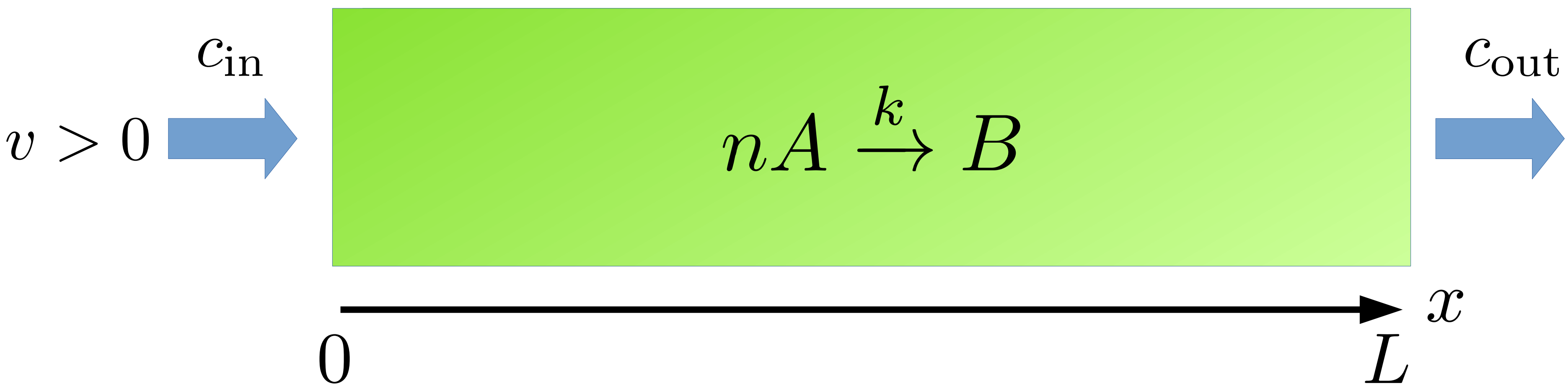
Tubular Reactor



Mass balance: $$\frac{\partial c}{\partial t} = D\frac{\partial^2 c}{\partial x^2} - v\frac{\partial c}{\partial x} - kc^n$$

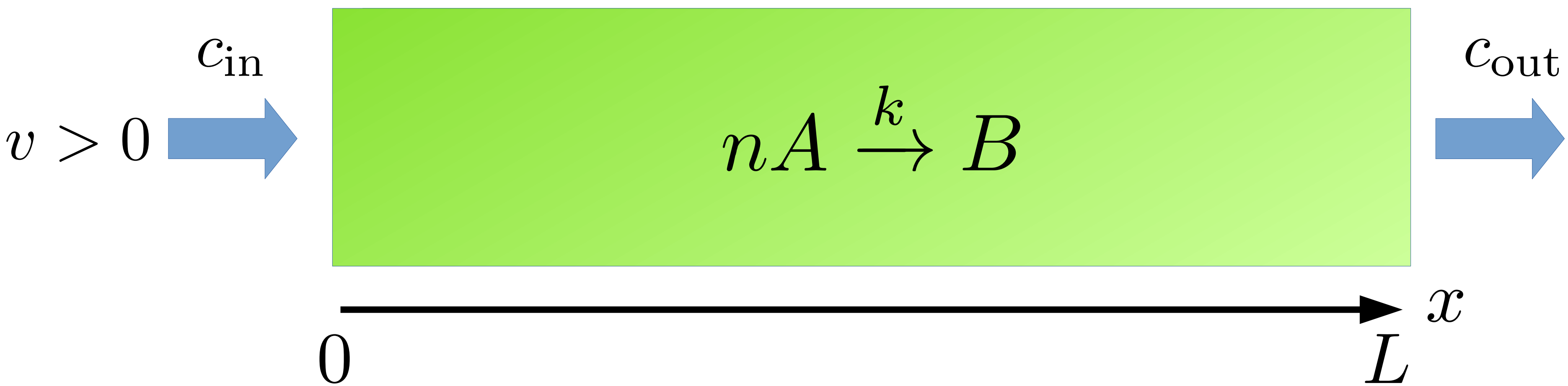
Reaction

Diffusion Advection/Convection

Boundary conditions: $$c(0) - \frac{D}{v}\frac{\partial c}{\partial x}(0) = c_{\text{in}} \qquad \frac{\partial c}{\partial x}(L) = 0$$

(Danckwerts)

Tubular Reactor



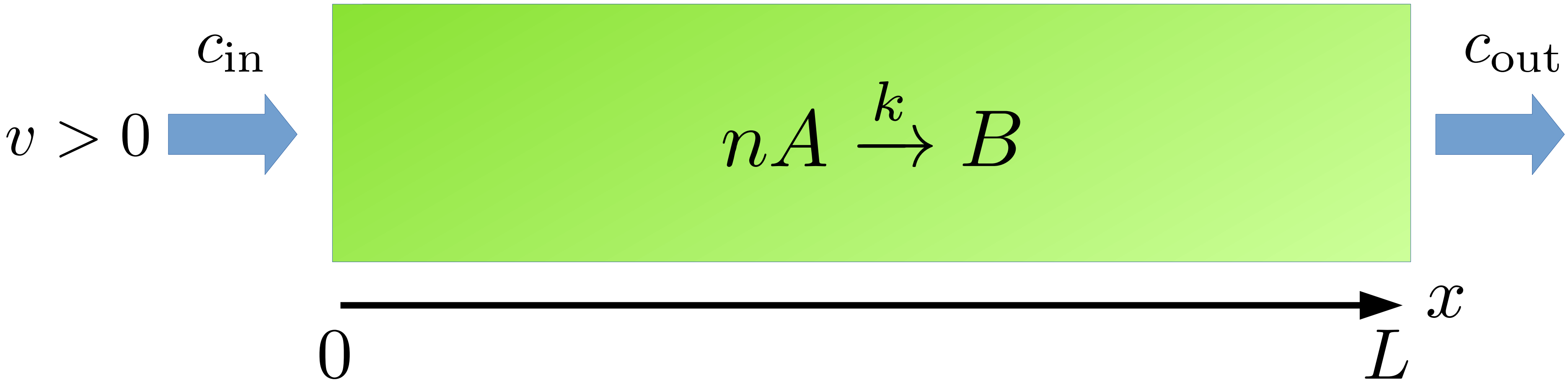
Mass balance: $$\frac{\partial c}{\partial t} = D\frac{\partial^2 c}{\partial x^2} - v\frac{\partial c}{\partial x} - kc^n$$

Non-dimensionalization: $$\theta = \frac{t}{\bar{t}} = \frac{tv}{L}$$

$$z = \frac{x}{L}$$

$$u = \frac{c}{c_{\text{in}}}$$

Tubular Reactor



Mass balance: $$\frac{\partial u}{\partial \theta} = \frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n$$

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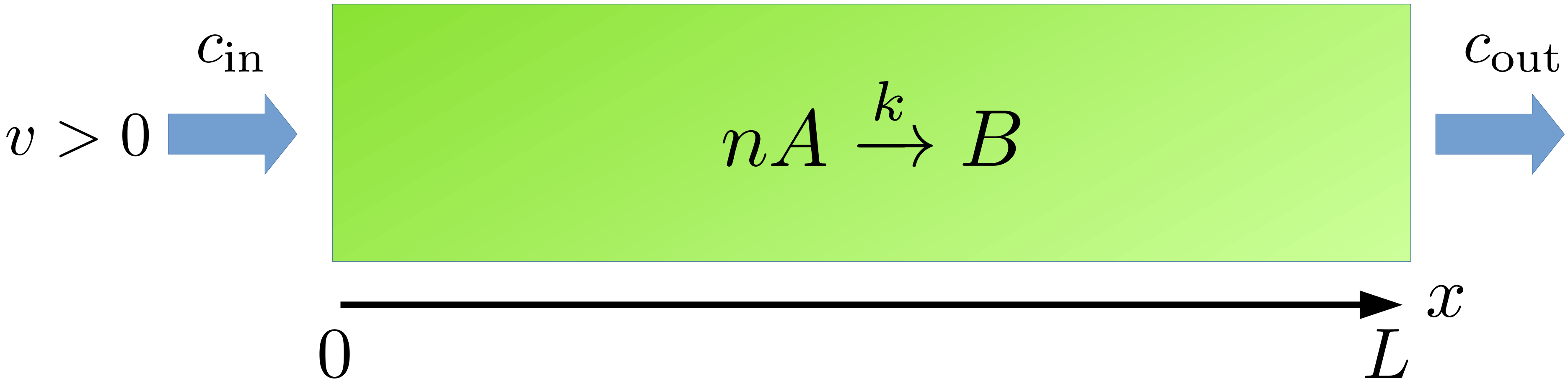
Tubular Reactor

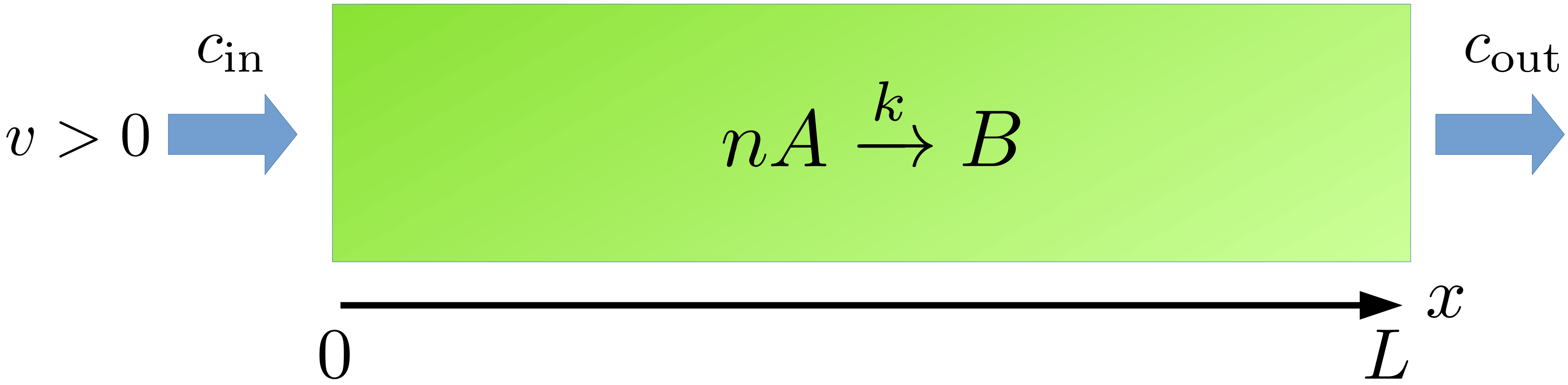


Mass balance: $$\frac{\partial u}{\partial \theta} = \frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n$$

Peclet number: $$Pe = \frac{L^2/D}{L/v} = \frac{\tau_{Diffusion}}{\tau_{Hydrodynamics}}$$

Damköhler number: $$Da = \frac{L/v}{1/(kc_0^{n-1})} = \frac{\tau_{Hydrodynamics}}{\tau_{Reaction}}$$

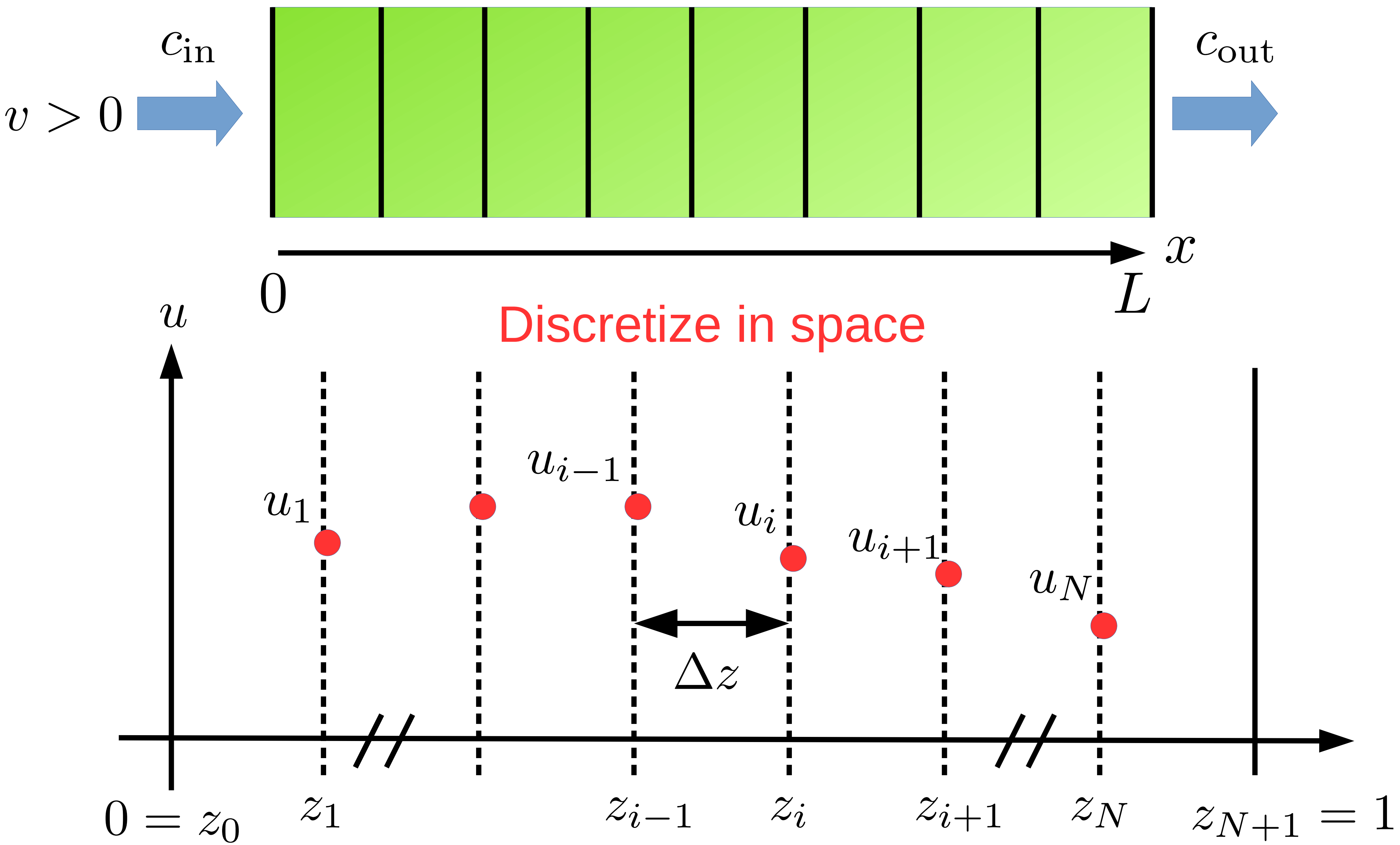
Tubular Reactor



Mass balance: $$\frac{\partial u}{\partial \theta} = \frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n = 0$$

Steady state tubular reactor

Tubular Reactor

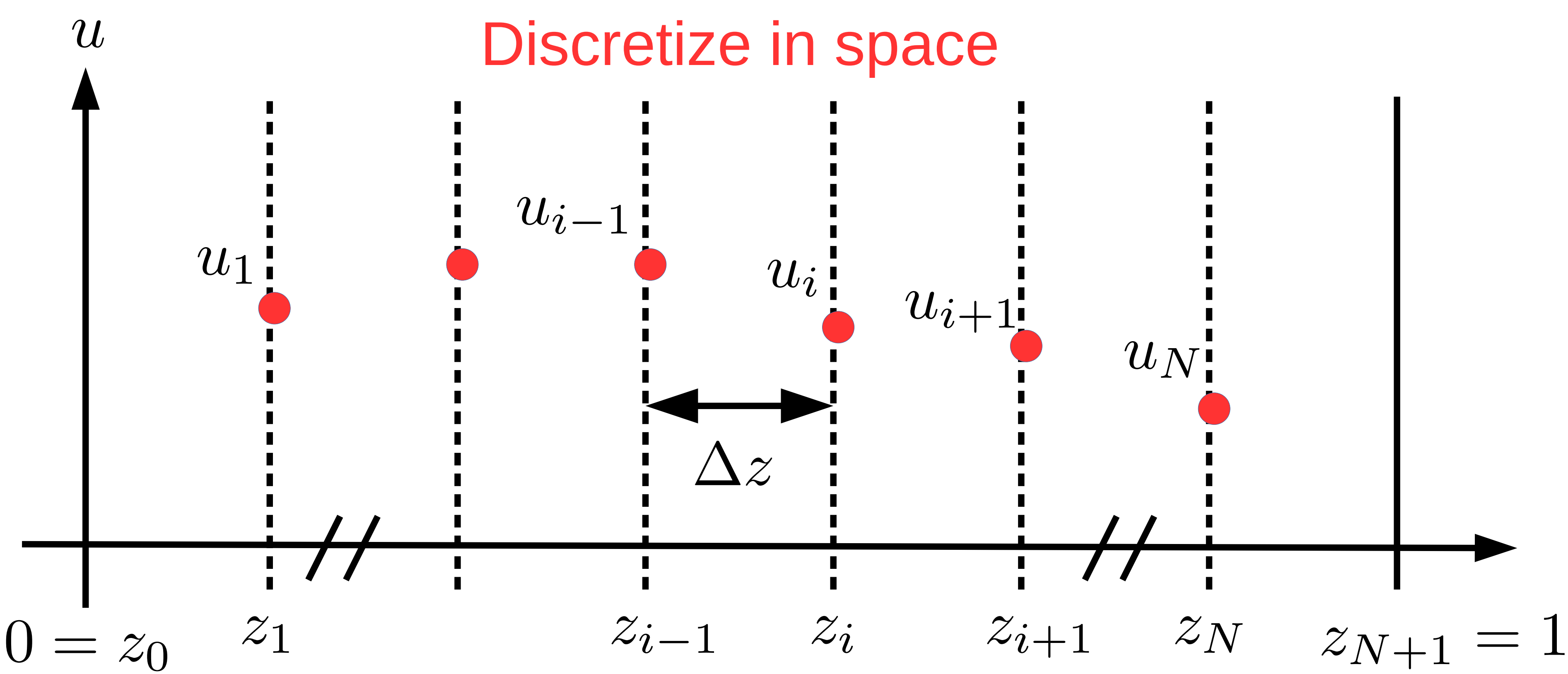


Tubular Reactor

$$\frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n = 0$$

$$\frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - Da \cdot u_i^n = 0$$

Discretize in space

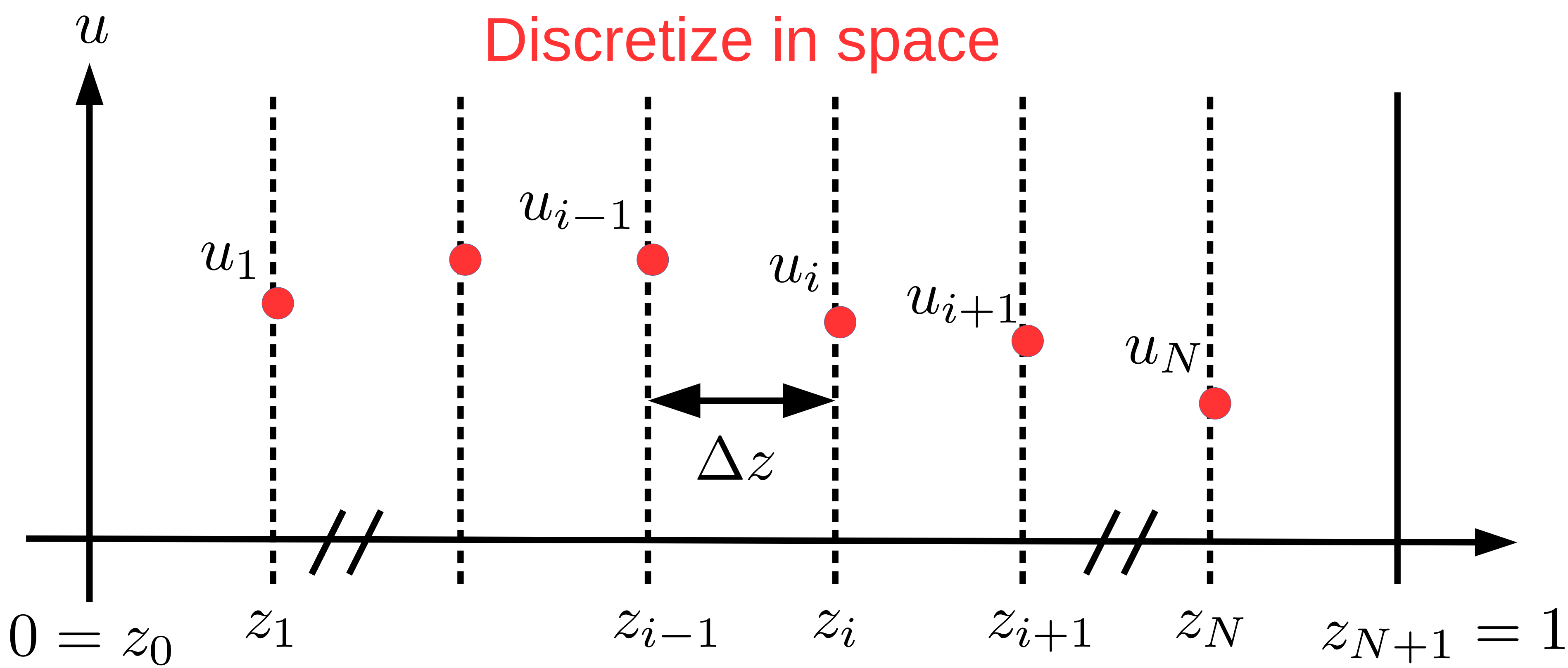


Tubular Reactor

Centered Finite Difference

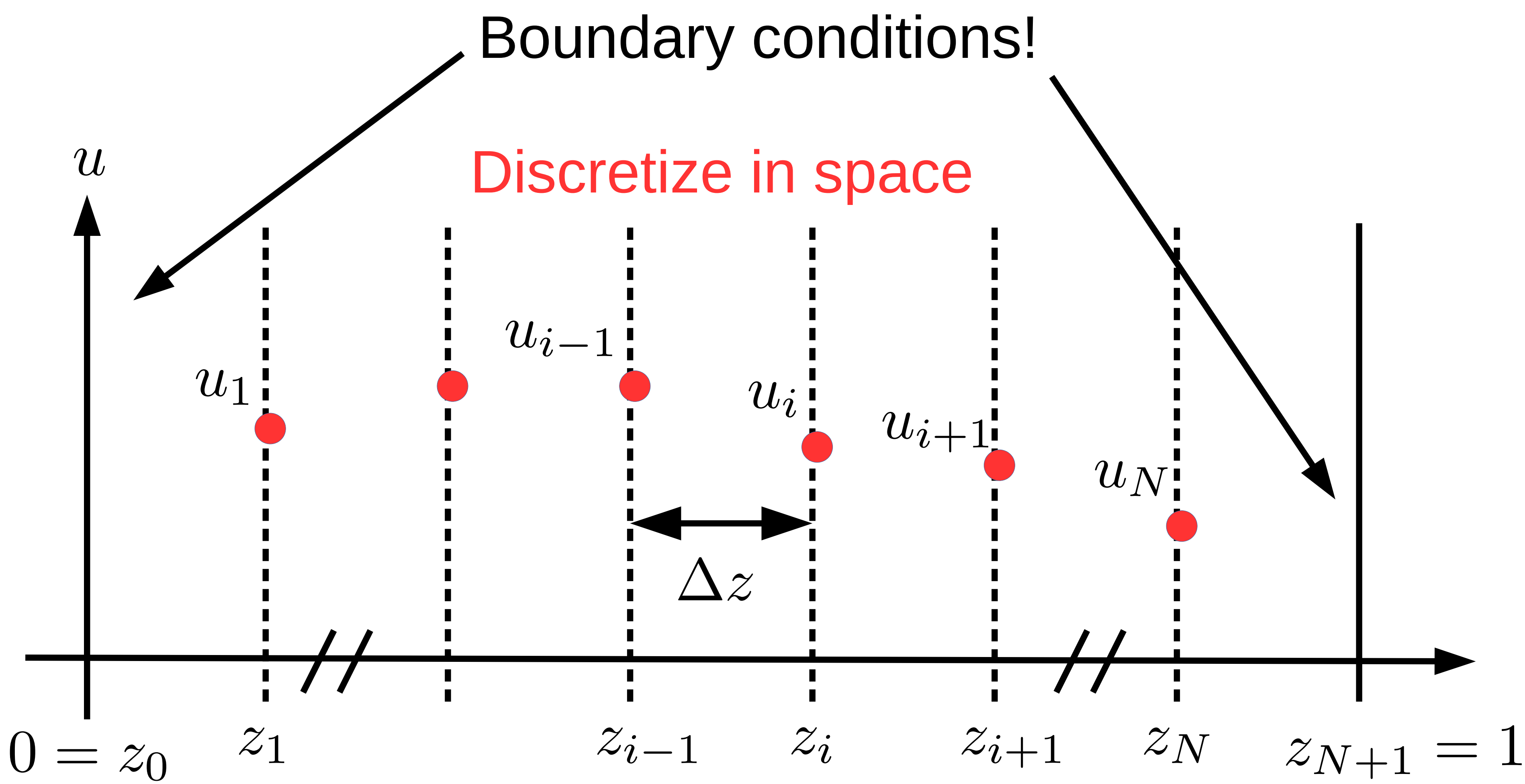
Backward Finite Difference

$$\frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - Da \cdot u_i^n = 0$$



Tubular Reactor

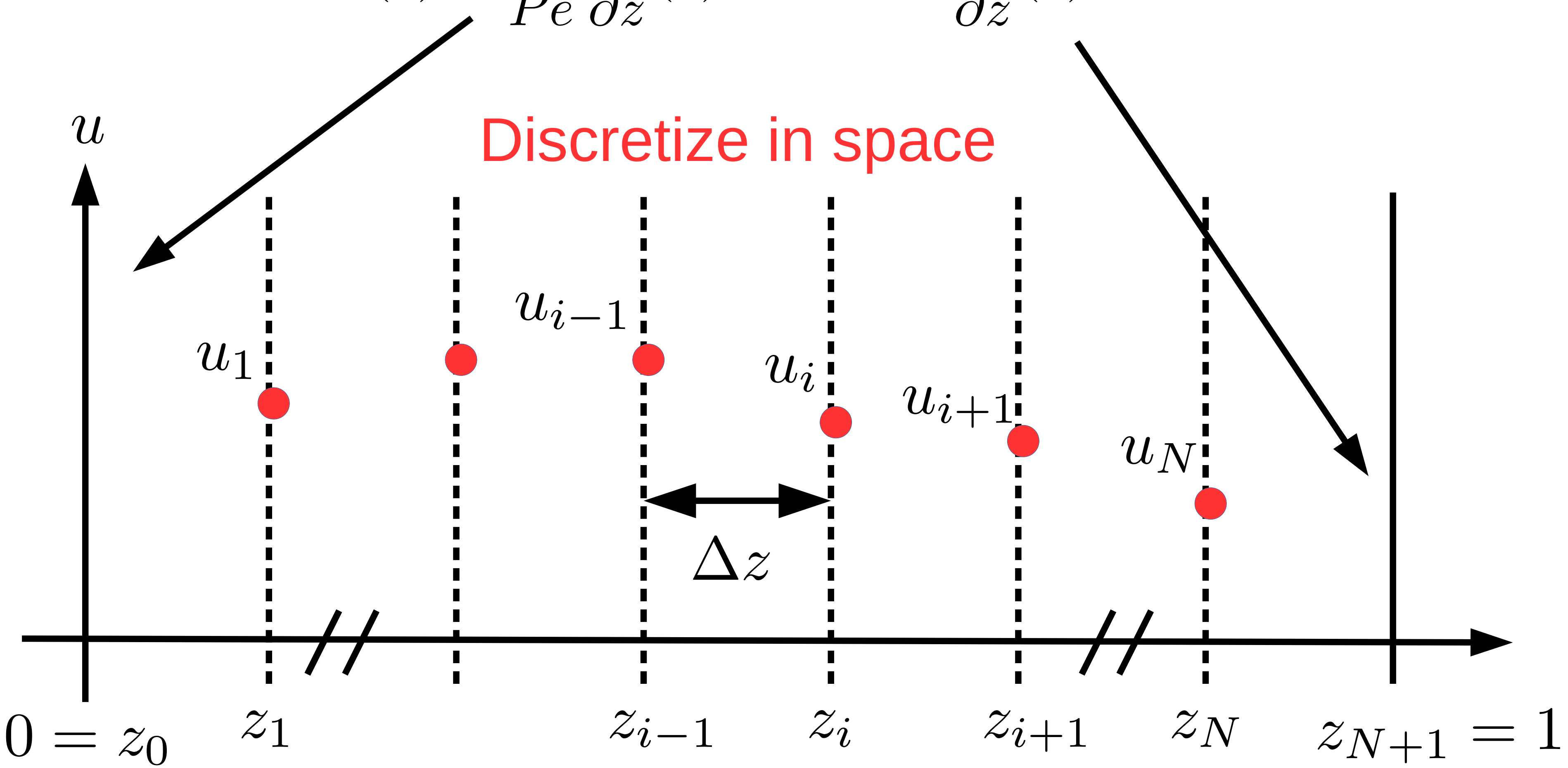
$$\frac{1}{Pe}\frac{u_{i+1}-2u_i+u_{i-1}}{\Delta z^2}-\frac{u_i-u_{i-1}}{\Delta z}-Da\cdot u_i^n=0$$



Tubular Reactor

$$\frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - Da \cdot u_i^n = 0$$

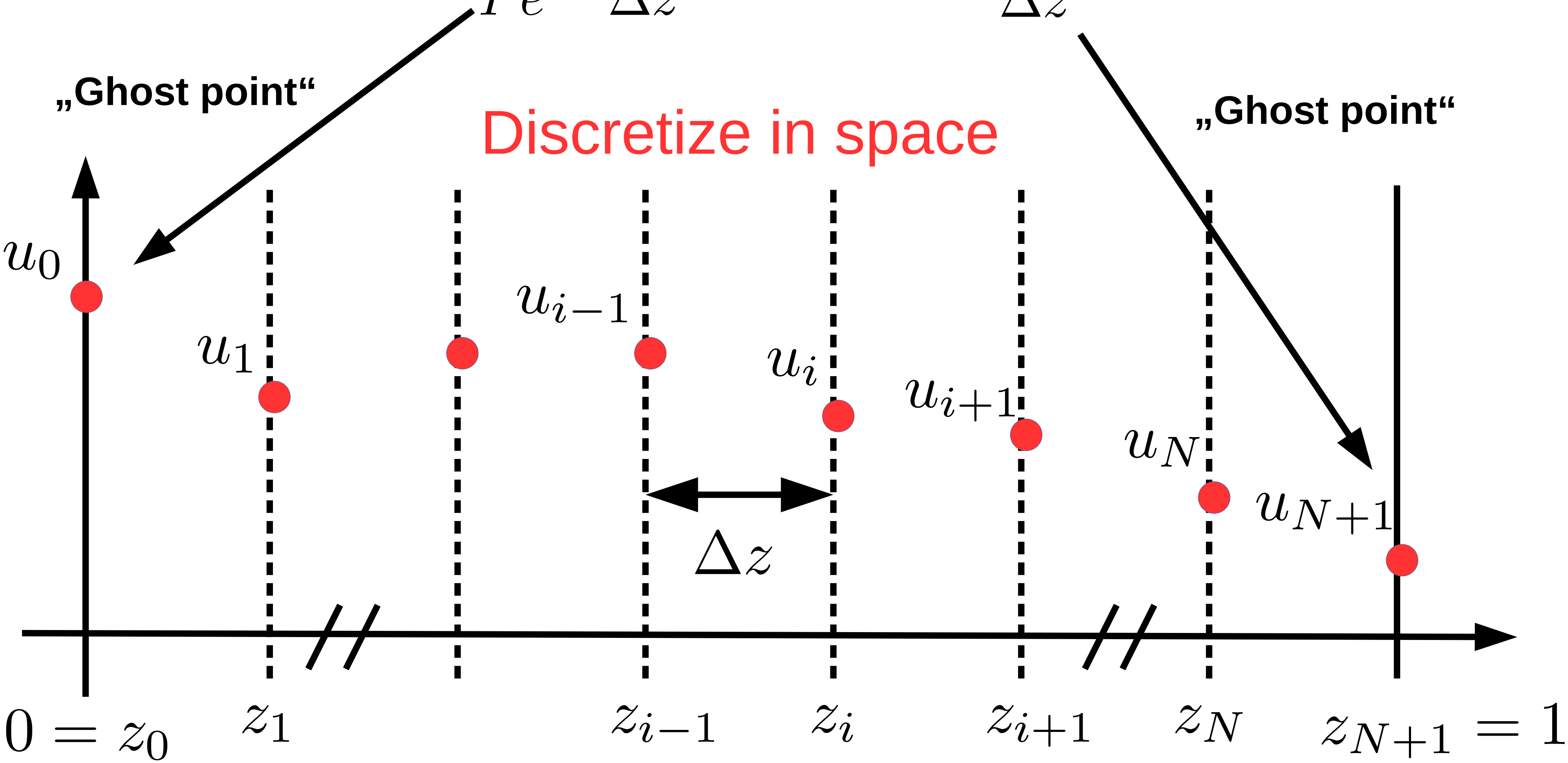
$$u(0) - \frac{1}{Pe}\frac{\partial u}{\partial z}(0) = 1 \qquad \frac{\partial u}{\partial z}(1) = 0$$



Tubular Reactor

$$\frac{1}{Pe}\frac{u_{i+1}-2u_i+u_{i-1}}{\Delta z^2}-\frac{u_i-u_{i-1}}{\Delta z}-Da\cdot u_i^n=0$$

$$u_0-\frac{1}{Pe}\frac{u_1-u_0}{\Delta z}=1 \qquad \frac{u_{N+1}-u_N}{\Delta z}=0$$



Tubular Reactor

$$\frac{1}{Pe}\frac{u_{i+1}-2u_i+u_{i-1}}{\Delta z^2}-\frac{u_i-u_{i-1}}{\Delta z}-Da\cdot u_i^n=0$$

$$u_0-\frac{1}{Pe}\frac{u_1-u_0}{\Delta z}=1 \longrightarrow u_0=\frac{1}{1+\frac{1}{Pe\Delta z}}\left(\frac{1}{Pe\Delta z}u_1+1\right)$$

$$\frac{u_{N+1}-u_N}{\Delta z}=0 \longrightarrow u_{N+1}=u_N$$

$$i=1,2,...,N$$

System of nonlinear equations!!!

Assignment 1

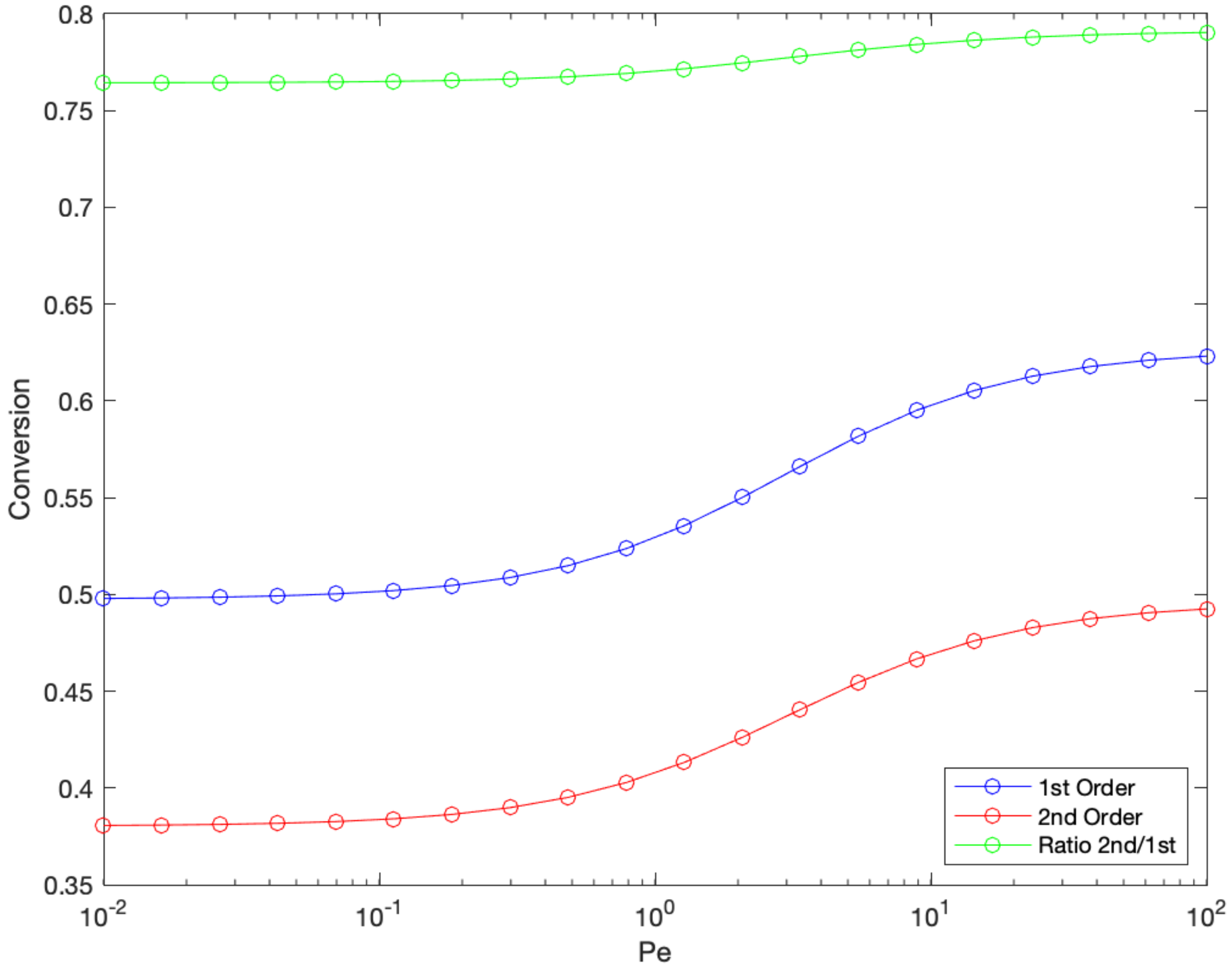
1. Solve the steady state tubular reactor for 20 different Peclet numbers (between 0.01 and 100) and for a first (n=1) and a second (n=2) order reaction. Use a Damköhler number of unity.
   Complete the template `rhs.m` by implementing the non-linear equations to solve.
2. Plot the conversion at the end of the reactor $1 - \frac{c_{\mathrm{out}}}{c_{\mathrm{in}}}$ vs. the Peclet number for both reaction orders.
   Also plot the ratio between the conversions of the first order and second order reaction

   •What is better for these reactions, a lot of back-mixing (Pe small, CSTR) or ideal plug flow (Pe large, PFR)?

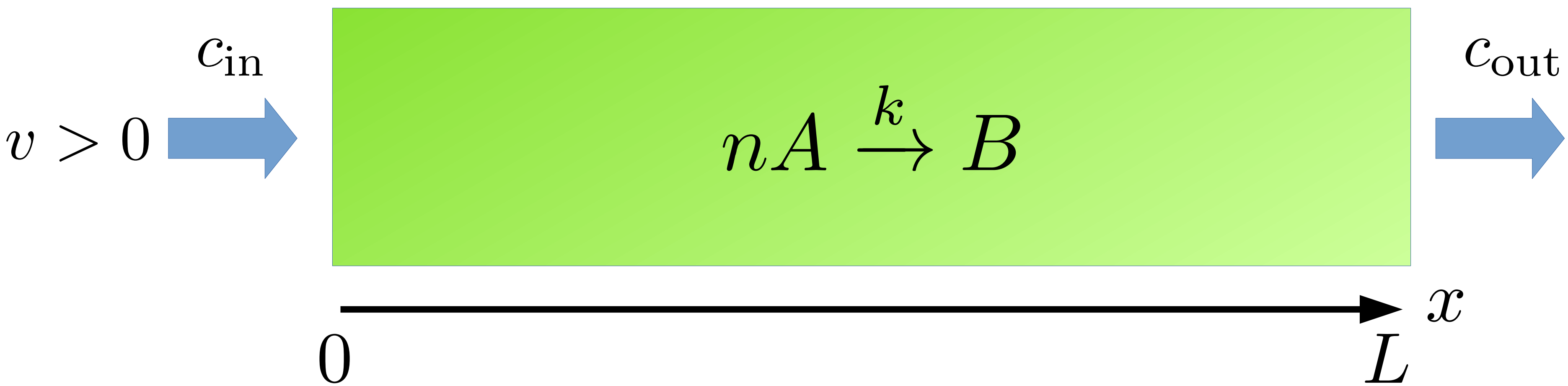
   •What influence does the reaction order have overall and at low or high Peclet numbers?

Complete the template `TubReact_steady_state.m`

Assignment 1



Tubular Reactor



Mass balance:

$$\frac{\partial c}{\partial t} = D\frac{\partial^2 c}{\partial x^2} - v\frac{\partial c}{\partial x} - kc^n$$

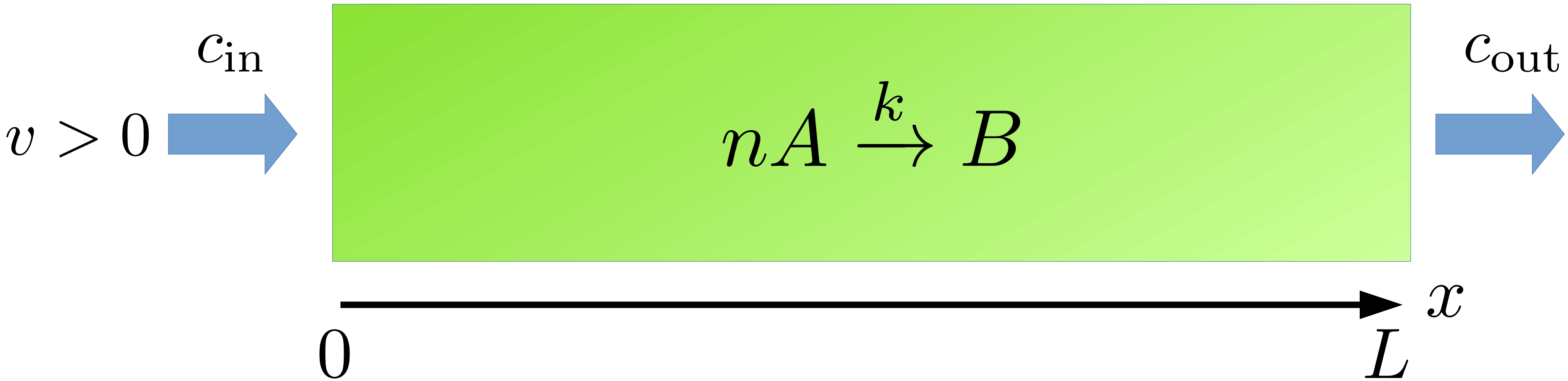
Reaction

Diffusion

Advection/Convection

Boundary conditions: $c(0) - \frac{D}{v}\frac{\partial c}{\partial x}(0) = c_{\text{in}} \qquad \frac{\partial c}{\partial x}(L) = 0$

Tubular Reactor



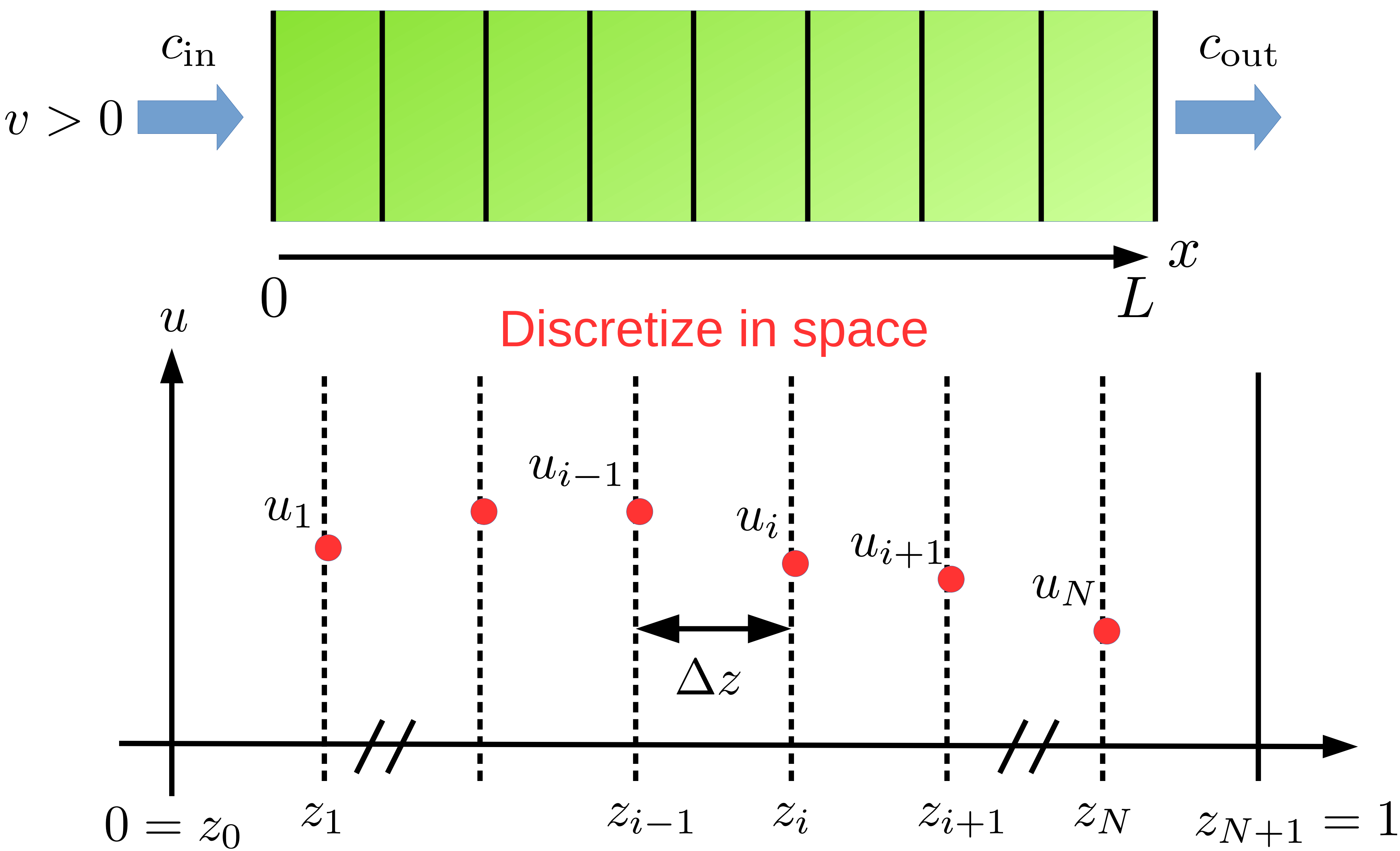
Mass balance:
$$\frac{\partial u}{\partial \theta} = \frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n$$

Dynamic tubular reactor

Boundary conditions:

$$u(0) - \frac{1}{Pe}\frac{\partial u}{\partial z}(0) = 1 \qquad \frac{\partial u}{\partial z}(1) = 0$$

Tubular Reactor

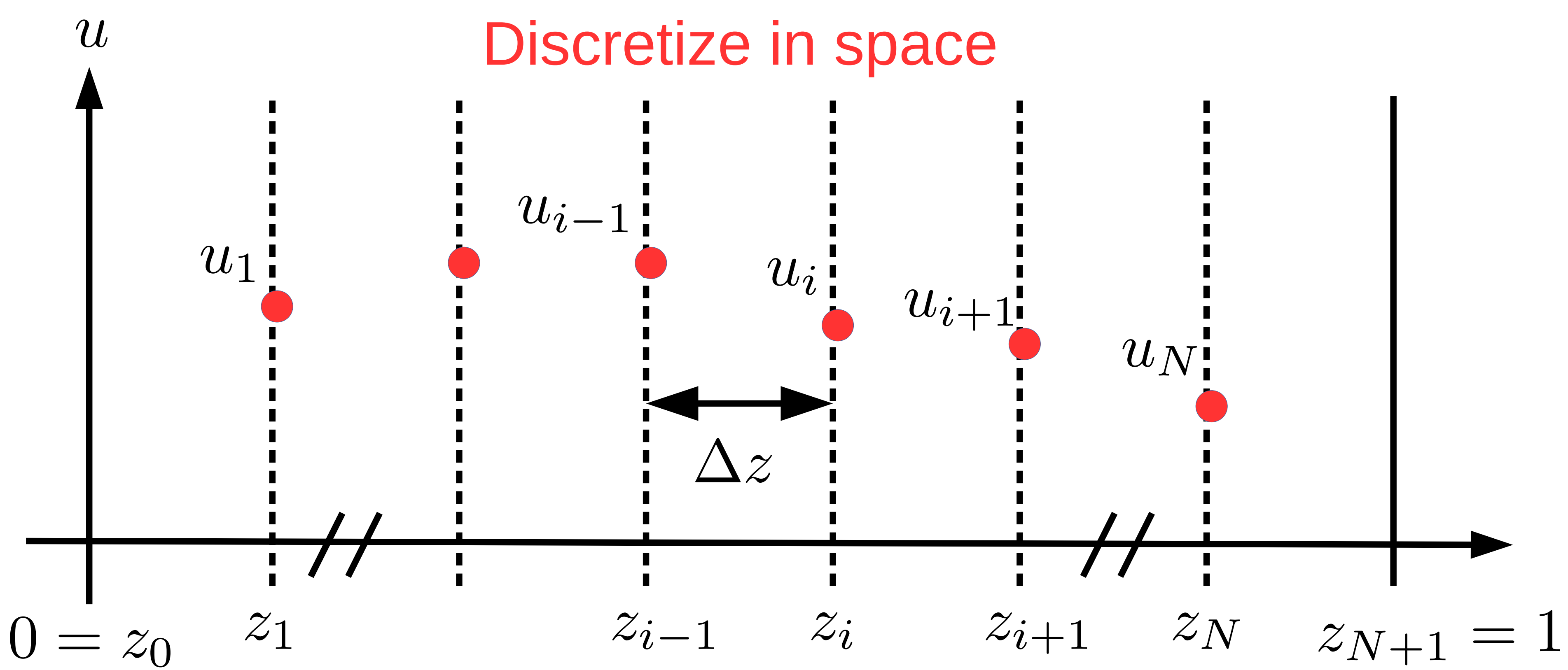


Tubular Reactor

$$\frac{\partial u}{\partial \theta} = \frac{1}{Pe}\frac{\partial^2 u}{\partial z^2} - \frac{\partial u}{\partial z} - Da \cdot u^n$$

ODEs $$\frac{\mathrm{d}u_i}{\mathrm{d}\theta} = \frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - k u_i^n$$

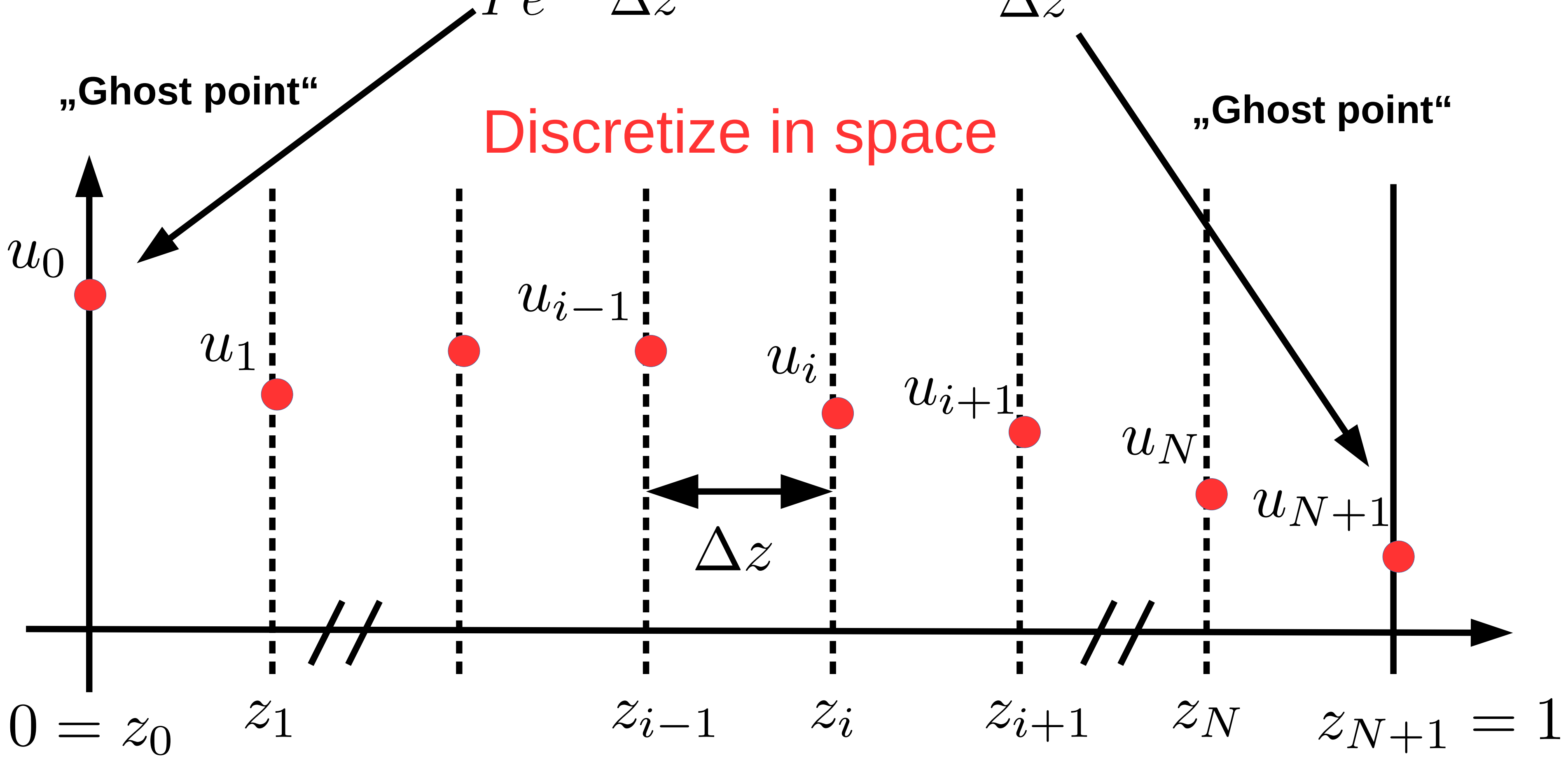
Discretize in space



Tubular Reactor

ODEs $$\frac{\mathrm{d}u_i}{\mathrm{d}\theta} = \frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - k u_i^n$$

$$u_0 - \frac{1}{Pe}\frac{u_1 - u_0}{\Delta z} = 1 \qquad \frac{u_{N+1} - u_N}{\Delta z} = 0$$

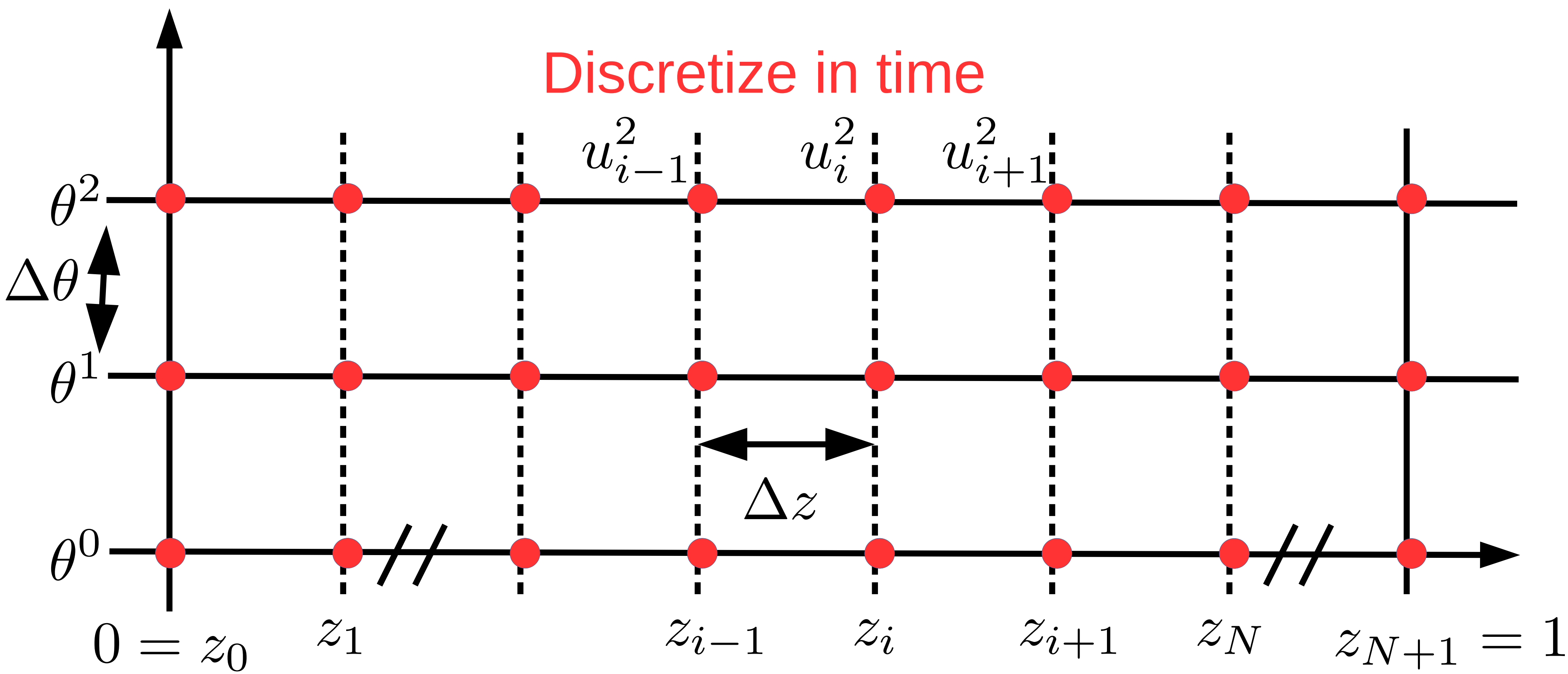


Tubular Reactor

Time index — Order of reaction

$$\frac{u_i^{n+1} - u_i^n}{\Delta\theta} = \frac{1}{Pe}\frac{u_{i+1}^n - 2u_i^n + u_{i-1}^n}{\Delta z^2} - \frac{u_i^n - u_{i-1}^n}{\Delta z} - k(u_i^n)^{\tilde{n}}$$

E.g. Explicit Euler, … But in general ver stiff



Tubular Reactor

$$\frac{\mathrm{d}u_i}{\mathrm{d}\theta} = \frac{1}{Pe}\frac{u_{i+1} - 2u_i + u_{i-1}}{\Delta z^2} - \frac{u_i - u_{i-1}}{\Delta z} - k u_i^n$$

$$u_0 - \frac{1}{Pe}\frac{u_1 - u_0}{\Delta z} = 1 \longrightarrow u_0 = \frac{1}{1 + \frac{1}{Pe\Delta z}}\left(\frac{1}{Pe\Delta z}u_1 + 1\right)$$

$$\frac{u_{N+1} - u_N}{\Delta z} = 0 \longrightarrow u_{N+1} = u_N$$

$$i = 1, 2, ..., N$$

System of nonlinear ODEs!!!
Stiff...

Assignment 2

1. Solve the dynamic tubular reactor from initial 0 to final time of 5 with MATLAB's `ode23s`

   Use the `rhs.m` from assignment 1 and the template `TubReact_dynamic.m`

   Consider only a first order reaction with Pe=100 and Da=1

2. Plot the conversion at the end of the reactor vs. dimensionless time

3. At what time does the solution reach a steady state, i.e. how many reactor volumes of solvent will you need?

Assignment 2